

Coupling an investment model with two sequential infrastructure models using Benders decomposition

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Agenda	UNIVERSITÄT DUISBURG ESSEN
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Motivation	1
Model	2
Data and cases	3
Results	4
Conclusion and outlook	
Conclusion and outlook	5



The role of hydrogen for the energy transition

Motivation – Model – Data and cases – Results – Conclusion and outlook

• Energy transition to reach climate neutrality major target of European energy policies

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- Hydrogen is seen as an important building block to reach these goals
 - Adressed for example in *REPower EU*
- European countries have developed hydrogen roadmaps with ambitious goals
 - E. g. Germany: National Hydrogen Strategy
- > Analyzing effects of hydrogen strategies requires integrated modelling approaches



Context: Ongoing research project MOPPL

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- "Model coupling (German: <u>Mo</u>dellko<u>ppl</u>ung) for the integrated optimization of long term transformation paths – coevolution, coordination and robustness under consideration of different system levels"
- Timeline
 - August 2022 July 2025
- Project Partners
 - ie3 (Technical University of Dortmund)
 - GWI Essen e.V. (Gas and heating institute Essen)
- Tasks
 - Integrated modelling of electricity, gas and hydrogen systems
 - Analysis of implications of different hydrogen strategies
 - Focus on the development of a mathematical approach to couple <u>independent</u> infrastructure models



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MOPPL: Benders Decomposition

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UNIVERSITÄT Challenges DUSSBURG **Open-**Minded **Motivation** – Model – Data and cases – Results – Conclusion and outlook 1. High level of detail of the 2. High number of 3. Subproblems not iterations in BD: subproblems (SP): independent of each Nodal simulations Especially if several other: technologies are Time step-coupling Dispatch from electricity restrictions (storage) endogenously optimized SP is input for the gas SP **Reduction in calculation and Research question I: Research question II:** How can BD be combined with Can subproblems be divided in running times: such a way that the optimal typical weeks and seasonal Simulation of only 4 typical storage modeling? solution of the integrated model is weeks (TWs) Enable parallelization of the Methodology developed, obtained? cf. Radek, Weber (2023) TWs Implement acceleration • techniques





- e. g. different weather years for the same operational subproblem
- ➤ parallelization possible

- Gas subproblem depends on elec. subproblem
- > no parallelization possible



UNIVERSITÄT **One integrated vs. two sequential subproblems** DEUSISEBURG **Open-**Minded Motivation – **Model** – Data and cases – Results – Conclusion and outlook **One integrated subproblem** Two sequential subproblems

- Electricity and H2 demand are served within one optimization
- Direct incentive for dispatch of electrolyzers through h2 demand constraint
 - Comparison between production costs and thirdcountry import price
- Direct incentive for dispatch of H2 power plants
 - No fuel costs necessary in input data
 - Consumption is part of H2 demand constraint \succ

- Electricity system is optimized prior to H2 system
- Incentivization by fixed H2 price (electricity) subproblem)
 - Incentive for electrolyzer dispatch through revenue generation
 - Incentive for H2 power plant dispatch by fuel costs —
- Gas subproblem
 - Seasonal H2 storages minimize third-country imports



Objective functions

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Master Problem:

min!
$$C^{M} = \sum_{r,i} c_{i}^{inv} \cdot K_{r,i} + \theta$$

Electricity subproblem:

$$min! \ C^{Op,Elec} = \sum_{tw,t,r,i} y_{tw,t,r,i} \cdot c_i^{var} \cdot freq_{tw} - \sum_{tw,t,r,iPtH2} y_{tw,t,r,iPtH2}^{H2} \cdot c^{H2} \cdot freq_{tw}$$
Revenue through H2 production

• Gas subproblem:

$$min! \ C^{Op,Gas} = \sum_{tw,t,r} \omega_{tw,t,r}^{H2} \cdot c^{H2} \cdot freq_{tw}$$

Parameters:

 c^{H2} – H2 import costs

Positive Variables: $\omega_{tw,t,r}^{H2}$ – Third country imports

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Third country import costs

Sets:

tw – Typical weeks

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- t Timesteps within a typical week
- r Regions

i – Technologies

Parameters:

 c_i^{inv} / c_i^{var} – Investment and variable costs $freq_{tw}$ – Frequency of typical week

Positive Variables:

 $K_{r,i}$ – Endogenously optimized capacities $y_{tw,t,r,i} / y_{tw,t,r,iPtH2}^{H2}$ – Electricity / H2 production

Integrated subproblem – Demand constraints

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• Electricity demand:

$$\sum_{i} y_{tw,t,r,i} + \sum_{iStoEl} y_{tw,t,r,iStoEl}^{dis} - \sum_{iStoEl} y_{tw,t,r,iStoEl}^{cha} - \sum_{iPtH2} y_{tw,t,r,iPtH2}^{cha} + \sum_{rr} (x_{tw,t,r,r}^{exp,el} - x_{tw,t,r,rr}^{imp,el}) + \omega_{tw,t,r} = D_{tw,t,r} \quad \forall tw, t, r$$
Elec. production Charging and discharging of elec storages Charging of electrolyzers Exports and imports Slack Exogenous demand

• H2 demand:

$$\sum_{iPtH2} y_{tw,t,r,iPtH2}^{H2} + \sum_{iH2} y_{tw,t,r,iH2}^{cons,H2} + \sum_{iStoH2} y_{tw,t,r,iStoH2}^{dis,H2} - \sum_{iStoH2} y_{tw,t,r,iStoH2}^{cha,H2} + \sum_{rr} (x_{tw,t,rr,r}^{exp,H2} - x_{tw,t,r,rr}^{imp,H2}) + \omega_{tw,t,r}^{H2} = D_{tw,t,r}^{H2} \quad \forall tw, t, r$$

$$H2 \text{ production and consumption} \quad \text{Charging and discharging of seasonal H2 storage} \quad \text{Exports and imports} \quad \text{Third} \quad \text{Exogenous demand country imports}$$

- Further constraints
 - Max. capacity, RES production, max. transmission capacities, H2 production, storage filling levels, ...



Sequential subproblems – Demand constraints

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• Electricity demand:

$$\sum_{i} y_{tw,t,r,i} + \sum_{isto \in I} y_{tw,t,r,isto \in I}^{dis} - \sum_{isto \in I} y_{tw,t,r,isto \in I}^{cha} - \sum_{iPH2} y_{tw,t,r,iPH2}^{cha} + \sum_{rr} (x_{tw,t,rr,r}^{exp,el} - x_{tw,t,r,rr}^{imp,el}) + \omega_{tw,t,r} = D_{tw,t,r} \quad \forall tw, t, r$$
Elec. production Charging and discharging of elec storages Charging of electrolyzers Exports and imports Slack Exogenous demand
$$H2 \text{ demand:}$$

$$\sum_{iPtH2} y_{tw,t,r,iPtH2}^{H2} + \sum_{iH2} y_{tw,t,r,iH2}^{cons,H2} + \sum_{isto H2} y_{tw,t,r,iSto H2}^{dis,H2} - \sum_{isto H2} y_{tw,t,r,iSto H2}^{cha,H2} + \sum_{rr} (x_{tw,t,rr,r}^{exp,H2} - x_{tw,t,r,rr}^{imp,H2}) + \omega_{tw,t,r}^{H2} = D_{tw,t,r}^{H2} \quad \forall tw, t, r$$

$$H2 \text{ production and consumption} \quad \text{Charging and discharging of seasonal H2 storage} \quad \text{Exports and imports} \quad \text{Third} \quad \text{Exogenous demand}$$

- Further constraints
 - Max. capacity, RES production, max. transmission capacities, H2 production, storage filling levels, ...



Master Problem: Benders Cuts

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j – Current iteration j' – Previous iterations

 γ – Optimality threshold

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 $\begin{aligned} \theta &\geq C_{j'}^{Op,Elec} + C_{j'}^{Op,Gas} \\ &+ \sum_{tw,t,r,iConv} \vartheta_{tw,t,r,iH2,j'}^{\max_cap} \cdot \left(K_{r,iH2,j} - K_{r,iH2,j'} \right) \\ &+ \sum_{tw,t,r,iPtH2} \vartheta_{tw,t,r,iPtH2,j'}^{\max_ptg} \cdot \left(K_{r,iPtH2,j} - K_{r,iPtH2,j'} \right) \\ &+ \dots \end{aligned}$

∀ j′

- θ is added to obj. fct. of master problem
- Dual values *θ* of capacity restrictions incentivize capacity adjustment in following iterations
- Added cuts reduce the solution space



Obj. fct. values of subproblems Cutting plane of H2 power plants

Cutting plane of electrolyzers (PtH2)

Potential further terms if capacities of more technologies are modelled endogenously



Integrated vs. sequential subproblems – solutions

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Main challenge: How to properly handle excess production of hydrogen in the elec. SP?

Naive approach:

Implementation of slack variable in H2 demand constraint of the gas SP

- Opposite of import variable
- Surplus is sold and revenues are subtracted in obj. function
- Influences obj. function value
- No direct influence on Benders cuts

Redispatch approach:

Implementation of electrolyzer redispatch in the gas SP

- Negative redispatch in surplus hours
- Elec. price from elec. SP as compensation
- Dual of redispatch capacity constraint added to Benders cut
- Influences obj. function value
- Direct influence on Benders cuts



Note:

We exclude *nested Benders* with inner iteration loop between subproblems because it would take to much time due to the expected amount of iterations.

UNIVERSITÄT **Redispatch approach** DEUSEBURG **Open-**Minded Motivation – **Model** – Data and cases – Results – Conclusion and outlook Adaption of objective function Elec. price from elec. SP $min! \ C^{Op,Gas} = \sum w_{tw,t,r}^{H2} \cdot c^{H2} \cdot freq_{tw} + \sum (y_{tw,t,r,iPtH2}^{RD+} - y_{tw,t,r,iPtH2}^{RD-}) \cdot p_{tw,t,r}^{el} \cdot freq_{tw}$ tw.t.r.iPtH2 New capacity constraint $\vartheta_{tw,t,r,iPtH2}^{max_pth2_rd}$ $y_{tw,t,r,iPtH2}^{cha,fix} + y_{tw,t,r,iPtH2}^{RD+} \le K_{r,iPtH2}^{0} + K_{r,iPtH2} \quad \forall tw,t,r,iPtH2 \mid$ Dual variable that is $y_{tw,t,r,iPtH2}^{cha,fix} - y_{tw,t,r,iPtH2}^{RD-} \ge 0 \quad \forall tw,t,r,iPtH2$ Elec. consumption of added to the Benders cut electrolyzer from elec. SP instead of the dual from the elec. SP

Adaption of H2 demand contraint

$$\sum_{iPtH2} (y_{tw,t,r,iPtH2}^{H2} + (y_{tw,t,r,iPtH2}^{RD+} - y_{tw,t,r,iPtH2}^{RD-}) \cdot eff_{iPtH2}) + \sum_{iH2} y_{tw,t,r,iH2}^{cons,H2} + \sum_{iStoH2} y_{tw,t,r,iStoH2}^{dis,H2} - \sum_{iStoH2} y_{tw,t,r,iStoH2}^{cha,H2} + \sum_{rr} (x_{tw,t,r,r,r}^{exp,H2} - x_{tw,t,r,rr}^{imp,H2}) + \omega_{tw,t,r}^{H2} = D_{tw,t,r}^{H2} \quad \forall tw, t, r$$

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Data and cases

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- Settings
 - Two regions (DE & FR)
 - Four typical weeks
 - tw_5, tw_22, tw_34 and tw_51
 - 168 time steps per week (hourly)
 - Simulation year 2045
- Cases
 - Base: Integrated optimization
 - Sequential subproblem
 - SeqSP_Naive: Seq. SP with naive correction
 - SeqSP_RD: Seq. SP with redispatch

- Scenario data
 - DE: Grid Expansion Plan (B 2045) *
 - FR: TYNDP 2022 Distributed Energy **
- Technologies
 - Endogenous capacity adjustment
 - Electrolyzers (PtH2)
 - H2 power plants
 - Exogenous capacities
 - Renewables (Wind onshore, W. offshore, PV, RoR)
 - Nuclear (only in FR)
 - Storage technologies (Batteries, Pump storage, Seasonal H2 storage)



* https://www.netzentwicklungsplan.de/sites/default/files/2023-01/Szenariorahmen_2037_Genehmigung.pdf ** https://2022.entsos-tyndp-scenarios.eu/download/

Results – Installed capacities

Motivation – Model – Data and cases – **Results** – Conclusion and outlook



- Both SeqSP variants yield optimal H2 power plant capacities
- Subtantial difference of > 30 GW in electrolyzer capacity for SeqSP_Naive





In SeqSP_RD, capacity difference decreases from > 30 GW to 2.4 GW

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Results – Electrolyzer dispatch

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Electrolyzer dispatch in Germany is approximated quite well Larger differences in France due to larger difference in installed capacity

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Summary

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> Sequential subproblems in expansion planning with Benders Decomposition pose challenges

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- > No integrated optimization of hydrogen production, consumption and storage
- > Obstacle of missing integration needs to be overcome by adaptions
- Naive approach converges, but results differ subtantially from integrated results
 excessive incentivization of electrolyzer capacity expansion due to overestimated revenues in gas SP
- > Redispatch approach promising, yet results still differ in a two-region case
 - > Iterative adaption of Benders cut with dual from gas SP leads to reasonable results
 - > No (strong) excessive incentivization due to handling of surplus hours



Conclusion and outlook

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Main findings

- Approach enables...
 - coupling of existing infrastructure models with an investment model in a sequential setting
 - integrated expansion planning of sector-coupled systems
- Approach beneficial...
 - when code owners cannot disclose proprietary information (e. g. full model code)
 - when integrated modeling of expansion planning in large system models computational too difficult

Outlook

- Further develop method to reduce remaining gap in a multi region / node case
- Application to more complex models
 - currently ongoing work in the project \rightarrow 39 regions case (NUTS2)

Remaining questions

• Can the remaining gap (in the multi-region case) be reduced or is it an error that has to be accepted?





Thank you for your attention

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